

Øving 10 - Erlend Sørli

1) a) $\Delta H^\circ = \sum \Delta H_f(\text{prod}) - \sum \Delta H_f(\text{reakt})$

$$\Delta H^\circ = \Delta H_f(\text{Si}_3\text{N}_4) - (\Delta H_f(\text{Si(s)}) + \Delta H_f(\text{N}_2(\text{g})))$$

$$\Delta H^\circ = (-743 - (2 \cdot 0 + 3 \cdot 0)) \text{ kJ/mol} = -743 \text{ kJ/mol}$$

Eksoberm, $\Delta H^\circ < 0$ * resten under

b) $q = c_p \cdot \Delta T = 100 \text{ J/(K}\cdot\text{mol)} \cdot (-1375 \text{ K}) = -137,5 \text{ kJ/mol}$

$$\Delta S = c_p \cdot \ln \frac{T_2}{T_1} = 100 \text{ J/(K}\cdot\text{mol)} \cdot \ln \frac{1673 \text{ K}}{298 \text{ K}} = 172,5 \text{ kJ}$$

$$T_1 = 298 \text{ K}$$

$$T_2 = 1673 \text{ K}$$

$$q = -137,5 \text{ kJ}, \Delta S = 172,5 \text{ kJ}$$

c) $n(\text{Si}_3\text{N}_4) = \frac{m(\text{Si}_3\text{N}_4)}{M_m(\text{Si}_3\text{N}_4)} = \frac{1000 \text{ g}}{190,15 \text{ g/mol}} = 7,127 \text{ mol}$

$$n(\text{N}_2) = 2 \cdot n(\text{Si}_3\text{N}_4) = 14,254 \text{ mol}$$

$$pV = nRT \Rightarrow V = \frac{nRT}{p} = \frac{14,254 \text{ mol} \cdot 8,314 \text{ J/(mol}\cdot\text{K)} \cdot 298 \text{ K}}{10^6 \text{ Pa}} = 0,036 \text{ m}^3$$

$$p = 10 \text{ bar} = 10^6 \text{ Pa}$$

$$V = 0,036 \text{ m}^3$$

a) * $\Delta G = \Delta G^\circ + RT \ln Q = \Delta G^\circ + RT \ln K = \Delta G^\circ$

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ$$

$$= 743 \text{ kJ/mol} - 1673 \text{ K} \cdot \Delta S^\circ$$

$$\Delta S^\circ = (101 - (31,9 + 2 \cdot 192)) = -310 \text{ J/K}\cdot\text{mol}$$

$$\Delta G^\circ = -743 \text{ kJ/mol} - 1673 \text{ K} \cdot (-310) \text{ J/K}\cdot\text{mol}$$

$$= -174 \text{ kJ/mol}$$

$$\Rightarrow \Delta G = -174 \text{ kJ/mol} < 0$$

\(\Rightarrow\) den er fortsatt spontan

2. Vi har formelen $\Delta G^\circ = -RT \ln K \Rightarrow K = e^{-\Delta G^\circ/RT}$

$$\frac{K_2}{K_1} = \frac{e^{-\Delta G_2^\circ/RT_2}}{e^{-\Delta G_1^\circ/RT_1}} = e^{-\Delta G_2^\circ/RT_2 - (-\Delta G_1^\circ/RT_1)}$$

$$\ln \frac{K_2}{K_1} = \frac{-\Delta G_2^\circ}{RT_2} + \frac{\Delta G_1^\circ}{RT_1} = -\frac{\Delta H^\circ}{RT_2} + \frac{\Delta S^\circ}{R} + \frac{\Delta H^\circ}{RT_1} - \frac{\Delta S^\circ}{R}$$

$$\ln \frac{K_2}{K_1} = -\frac{\Delta H^\circ}{RT_2} + \frac{\Delta H^\circ}{RT_1} = -\frac{\Delta H^\circ}{R} \left(\frac{1}{T_2} - \frac{1}{T_1} \right)$$

$$\underline{\underline{\ln \frac{K_2}{K_1} = -\frac{\Delta H^\circ}{R} \left(\frac{1}{T_2} - \frac{1}{T_1} \right)}}$$

3 $K = \frac{a_{\text{Na}_2\text{CO}_3} \cdot a_{\text{H}_2\text{O}} \cdot a_{\text{CO}_2}}{a_{\text{NaHCO}_3}^2} = a_{\text{H}_2\text{O}} \cdot a_{\text{CO}_2} = 0,231$

a_i for solids = 1

$$\frac{p_{\text{H}_2\text{O}}}{p_{\text{ref}}} \cdot \frac{p_{\text{CO}_2}}{p_{\text{ref}}} = 0,231 p_{\text{ref}}^2$$

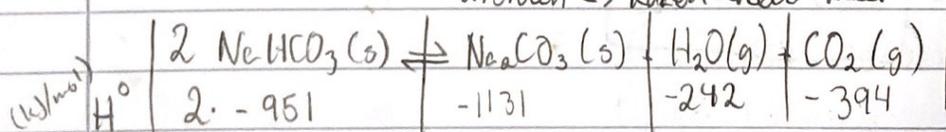
Siden $n(\text{H}_2\text{O}) = n(\text{CO}_2)$

$$p^2 = 0,231 p_{\text{ref}}^2$$

$$\Rightarrow p(\text{H}_2\text{O}) p(\text{CO}_2) = 1$$

$$p = 0,481 p_{\text{ref}}$$

$p < p_{\text{ref}} \Rightarrow$ Trykket av gassene inne i kaken er mindre enn utsiden \Rightarrow kaken hever ikke.



$$\Rightarrow \Delta H^\circ = 135 \text{ kJ/mol} \Rightarrow \text{endoterm rx}$$

Steketemperatur $> 100^\circ\text{C}$ anbefales fordi at ved 100°C er ikke gasstrykket dannet av bakepulver høyt nok til at kaken heves. Siden reaksjonen er endoterm, vil vi få økt gassdannelse ved å øke temperaturen (gass er produkter), dette vil øke gasstrykket inni kaken og ved stor nok økning vil kaken heve.

4) fra sl for CH_3Cl er: $\Delta H_f^\circ = -82 \text{ kJ/mol}$
 $S^\circ = 235 \text{ J/(K}\cdot\text{mol)}$
 $\Delta_{\text{vap}}H = 22 \text{ kJ/mol}$
 $t_b = -24,2^\circ\text{C} = 248,9 \text{ K}$

Fra (l) til (g):

$$\Delta H_{\text{rx}} = \Delta H_{\text{vap}} = \Delta H_f^\circ(\text{gass}) - \Delta H_f^\circ(\text{væske})$$

$$\Rightarrow \Delta H_f^\circ(\text{væske}) = \Delta H_f^\circ(\text{gass}) - \Delta H_{\text{vap}} = (-82 - 22) \text{ kJ/mol} = -104 \text{ kJ/mol}$$

For faseoverganger er $\Delta S = \frac{-\Delta_{\text{vap}}H}{t_b} = \frac{22 \cdot 10^3 \text{ J/mol}}{248,9 \text{ K}} = 88,4 \text{ J/(mol}\cdot\text{K)}$

$$S^\circ_{\text{væske}} = S^\circ_{\text{gass}} - \Delta S = (235 - 88,4) \text{ J/(mol}\cdot\text{K)} = 147 \text{ J/(mol}\cdot\text{K)}$$

$$\underline{\underline{H_f^\circ = -104 \text{ kJ/mol} \quad S^\circ = 147 \text{ J/(K}\cdot\text{mol)}}$$

5) a) $W = -P_{\text{ekst}} \cdot \Delta V$
 $q = -W = P_{\text{ekst}} \cdot \Delta V$

$W = -P_{\text{ekst}} \cdot \Delta V, \quad q = P_{\text{ekst}} \cdot \Delta V$

b) $W_{D \rightarrow A} = W_{D \rightarrow B} + W_{B \rightarrow A} = 0 + (P_A \Delta V) = -P_A(V_A - V_B)$
 $q_{D \rightarrow A} = P_A(V_A - V_B) \quad V_B > V_A \Rightarrow \text{Varme forlater systemet}$
 $W = -P_A(V_A - V_B)$

c) $q_{D \rightarrow A} = q_{A \rightarrow C} + q_{C \rightarrow D} + q_{D \rightarrow B} + q_{B \rightarrow A} = 0 + P_C(V_D - V_C) + 0 + P_A(V_A - V_B)$
 $|V_D - V_C| = |V_A - V_B|$ og $P_A > P_C \Rightarrow |P_C(V_D - V_C) + P_A(V_A - V_B)| < 0$
 \Rightarrow Varme tilført systemet er $< 0 \Rightarrow$ Varme tilført omgivelsene > 0
 $\Rightarrow \Delta S_{\text{omg}} = -\frac{q_{\text{omg}}}{T} = \frac{q_{\text{omg}}}{T} > 0, \quad q_{\text{omg}} = -q_{\text{system}}$
 $\Rightarrow \Delta S_{\text{omg}} = -\frac{P_C(V_D - V_B) + P_A(V_A - V_B)}{T}$

Boltzmanns $\Delta S = k_B \ln \frac{W_f}{W_i}$ alle makrotilstander er like $\Rightarrow \Delta S = \ln 1 = 0$

2. lov $\Rightarrow \Delta S_{\text{univ}} = \Delta S_{\text{omg}} + \Delta S_{\text{system}} = \Delta S_{\text{omg}} \quad (\Delta S_{\text{system}} = 0)$
 $\Rightarrow \underline{\underline{\Delta S_{\text{univ}} = \Delta S_{\text{omg}} > 0}}$ (irreversibel prosess)

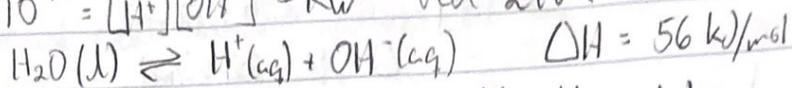
$\Delta S_{\text{system}} = 0$

d) reversibel prosess $\Rightarrow q_{\text{rev}} = 0 \Rightarrow \Delta S = \frac{-q_{\text{rev}}}{T} = \frac{0}{T} = 0, \underline{\underline{\Delta S = 0}}$

6

$$14 = pOH + pH$$

$$10^{-14} = [H^+][OH^-] = K_w \text{ ved } 298K$$



ved å tilføre varme forskyves likevekten mot høyre.

Vi bruker formel fra 2: (Vi definerer Q som K_w for $70^\circ C = 343K$)

$$\ln \frac{Q}{K_w} = -\frac{\Delta H}{R} \left(\frac{1}{T_2} - \frac{1}{T_1} \right)$$

$$= -\frac{56 \text{ kJ/mol}}{8,314 \text{ J/K}\cdot\text{mol}} \left(\frac{1}{343K} - \frac{1}{298K} \right) = 2,965$$

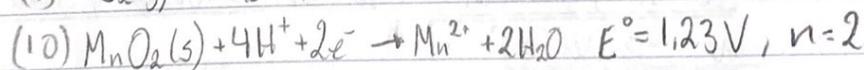
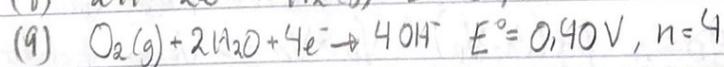
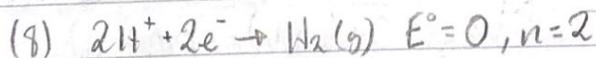
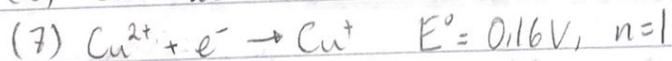
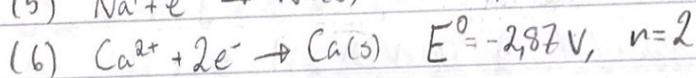
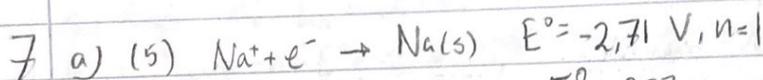
$$\frac{Q}{K_w} = e^{2,965}$$

$$Q = e^{2,965} \cdot 10^{-14} = 1,94 \cdot 10^{-13}$$

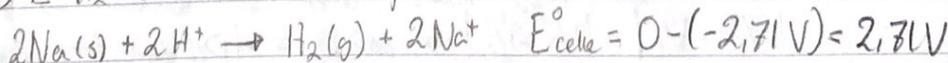
$$[H^+] = \sqrt{Q} \Rightarrow pH = -\log \sqrt{Q} = 6,35$$

$$K_w = [OH^-] \cdot [H^+] \Rightarrow -\log K_w = pOH + pH$$

$$\Rightarrow 12,7 = pOH + pH, \quad \underline{pH(70^\circ C) = 6,35}$$



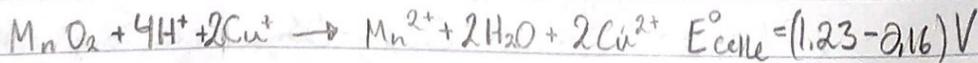
b) $E^\circ_{H_2}$ er størst \Rightarrow reduksjon



(Antar at det er standard cellepotensial oppgaven ber om siden vi mangler konsentrasjoner.) (Antar vi $Q=1$ er uansett $E^\circ_{\text{celle}} = E_{\text{celle}}$)

i) $\underline{E^\circ_{\text{celle}} = 2,71 \text{ V}}$

$E^\circ_{MnO_2(s)}$ er størst, det reduseres

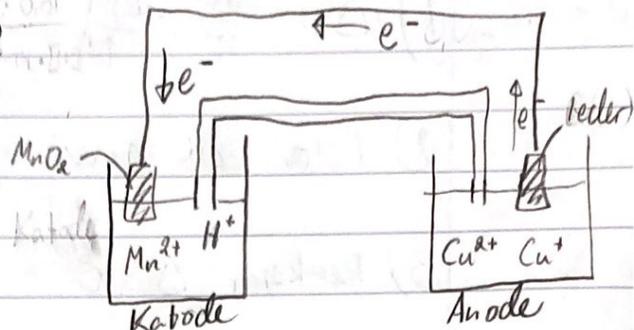


$$\underline{E^\circ_{\text{celle}} = 1,07 \text{ V}}$$

$$7 \quad c) \quad E_{\text{celle}} = E^{\circ}_{\text{celle}} - \frac{RT}{nF} \cdot \ln Q$$

$$[H^+] = \sqrt{K_w} = 10^{-7}$$

$$Q = \frac{0,1^2 \cdot 0,01}{0,01^4 (10^{-7})^4} = 10^{28}$$



$$E_{\text{celle}} = 1,07V - \frac{R \cdot 298K}{2 \cdot \text{mol} \cdot F} \cdot \ln 10^{28} = 0,242V = \underline{0,242mV}$$

(Tar kritikk på anoden er på høyre side istedet for venstre, skissen skulle vært speilet)

$$\underline{E_{\text{celle}} = 0,242mV}$$

8 a) Det er $F_2(g)$ ettersom $E^{\circ}(F_2)$ er størst

b) $F_2(g)$ og $H_2O_2(aq)$, de har $E^{\circ} > E^{\circ}(PbO_2)$

c) ingen av dem, de har alle $E^{\circ} < E^{\circ}(F_2)$